

eau:  $P_1 = 1 \text{ MPa}$        $P_2 = 1 \text{ MPa}$   
 $T_1 = 300^\circ\text{C}$        $T_2 = 100^\circ\text{C}$   
 $\dot{V}_1 = 1 \frac{\text{m}^3}{\text{s}}$        $\dot{m}_2 = 1 \frac{\text{kg}}{\text{s}}$

$P_3 = 1 \text{ MPa}, A_3 = 0.1 \text{ m}^2$

air:  $\dot{m}_a = 30 \text{ kg/s}$   
 $T_4 = 20^\circ\text{C}$        $T_5 = 60^\circ\text{C}$   
 $\mathcal{V}_4 = 3 \text{ m/s}$        $\mathcal{V}_5 = 7 \text{ m/s}$

- régime permanent
- air  $\rightarrow$  gaz parfait à  $C_p, C_v$  const.  
 $R = 0.287 \frac{\text{kPa}\cdot\text{m}^3}{\text{kg}\cdot\text{K}}, C_p = 1.005 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$
- $\dot{Q}_{\text{ext}} \approx 0$
- $\Delta e_{\text{air}}, \Delta e_{\text{eau}}, \Delta e_{\text{eau}} = 0$

a)  $T_3, x_3 = ?$

b)  $\dot{Q}_{\text{ea}} = ?$

c)  $\mathcal{V}_3 = ?$

Suppositions additionnelles: aucune

a)  $T_3, x_3$ : on a  $P_3$ , il faut trouver  $h_3$  pour définir l'état ③

i) conservation de la masse:  $\sum \dot{m}_{\text{in}} = \sum \dot{m}_{\text{out}}$  (régime perm.)

eau:  $\dot{m}_1 + \dot{m}_2 = \dot{m}_3$

air:  $\dot{m}_4 = \dot{m}_5 = \dot{m}_a$

ii) bilan d'énergie (1<sup>ère</sup> loi):  $\dot{E}_{\text{in}} = \dot{E}_{\text{out}}$  (régime perm.)

$\dot{m}_1 \theta_1 + \dot{m}_2 \theta_2 + \dot{m}_4 \theta_4 + \dot{W}_e = \dot{m}_3 \theta_3 + \dot{m}_5 \theta_5$   
 $\dot{m}_1 \theta_1 + \dot{m}_2 \theta_2 + \dot{m}_a \theta_4 + \dot{W}_e = (\dot{m}_1 + \dot{m}_2) \theta_3 + \dot{m}_a \theta_5$   
 $\dot{m}_1 (\theta_3 - \theta_1) + \dot{m}_2 (\theta_3 - \theta_2) = \dot{m}_a (\theta_4 - \theta_5) + \dot{W}_e$

$\dot{m}_1 (h_3 - h_1 + \cancel{\Delta e_{u13}} + \cancel{\Delta e_{p13}}) + \dot{m}_2 (h_3 - h_2 + \cancel{\Delta e_{c23}} + \cancel{\Delta e_{p23}}) = \dot{m}_a (h_4 - h_5 + \frac{\mathcal{V}_4^2 - \mathcal{V}_5^2}{2} + \cancel{\Delta e_{p54}}) + \dot{W}_e$

$(\dot{m}_1 + \dot{m}_2) h_3 = \dot{m}_1 h_1 + \dot{m}_2 h_2 - \dot{m}_a (h_5 - h_4 + \frac{\mathcal{V}_5^2 - \mathcal{V}_4^2}{2}) + \dot{W}_e$

$\Rightarrow h_5 - h_4 = C_p (T_5 - T_4)$  (gaz parfait)

Note:  $\Delta h = C_p \Delta T$  mais  $h \neq C_p T$   
 excepté pour un gaz caloriquement parfait

$$h_3 = \frac{\dot{m}_1 h_1 + \dot{m}_2 h_2 - \dot{m}_a \left[ c_p (T_5 - T_4) + \frac{v_5^2 - v_4^2}{2} \right] + \dot{W}_e}{\dot{m}_1 + \dot{m}_2}$$

$\Rightarrow h_1 = ? : P_1 = 1000 \text{ kPa}$   
 $T_1 = 300^\circ\text{C}$

$T_1 > T_{\text{sat}@1000 \text{ kPa}} \stackrel{\text{A-5}}{=} 179.88^\circ\text{C} \rightarrow \text{vapeur surchauffée}$   
 Table A-6:  $h_1 = 3051.6 \frac{\text{kJ}}{\text{kg}}$   
 $(v_1 = 0.25799 \text{ m}^3/\text{kg})$

$\Rightarrow h_2 = ? : P_2 = 1000 \text{ kPa}$   
 $T_2 = 100^\circ\text{C}$

$T_2 < T_{\text{sat}@1000 \text{ kPa}} \stackrel{\text{A-5}}{=} 179.88 \rightarrow \text{liquide comprimé}$   
 $h_2 \approx h_f @ 100^\circ\text{C} \stackrel{\text{A-4}}{=} 419.17 \text{ kJ/kg}$

$\Rightarrow \dot{m}_1 = \frac{\dot{V}_1}{v_1} = \frac{1 \text{ m}^3/\text{s}}{0.25799 \text{ m}^3/\text{kg}} = 3.876 \text{ kg/s}$

$$h_3 = (3.876 \frac{\text{kg}}{\text{s}}) (3051.6 \frac{\text{kJ}}{\text{kg}}) + (1 \frac{\text{kg}}{\text{s}}) (419.17 \frac{\text{kJ}}{\text{kg}}) - (30 \frac{\text{kg}}{\text{s}}) \left[ (1.005 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}) (60 - 20)^\circ\text{C} \cdot \frac{\text{K}}{^\circ\text{C}} + \frac{(7^2 - 3^2)}{2} \frac{\text{m}^2}{\text{s}^2} \cdot \frac{1 \text{ kJ/kg}}{10^3 \frac{\text{m}^2}{\text{s}^2}} \right] + 10.6 \frac{\text{kJ}}{\text{s}}$$


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(3.876 + 1) kg/s

$h_3 = 2266.44 \text{ kJ/kg}$

L'état ③ est donc défini par  $P_3 = 1000 \text{ kPa}$  &  $h_3 = 2266.44 \frac{\text{kJ}}{\text{kg}}$

Table A-5: Pour  $P_{\text{sat}} = 1000 \text{ kPa}$ ,  $T_{\text{sat}@1000 \text{ kPa}} = 179.88^\circ\text{C}$

$h_f = 762.51 \frac{\text{kJ}}{\text{kg}}$      $h_{fg} = 2014.6 \frac{\text{kJ}}{\text{kg}}$   
 $h_g = 2777.1 \frac{\text{kJ}}{\text{kg}}$

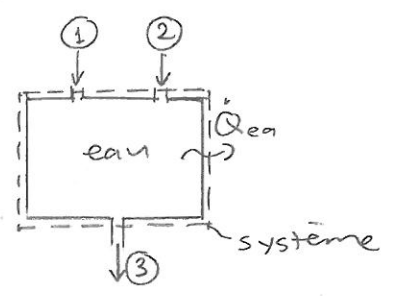
$h_f < h_3 < h_g \rightarrow$  mélange liquide-vapeur saturé

$T_3 = T_{\text{sat}@1000 \text{ kPa}} = \boxed{179.88^\circ\text{C}}$

$x_3 = \frac{h_3 - h_f}{h_{fg}} = \frac{2266.44 - 762.51}{2014.6} = \boxed{0.7465}$

Solution alternative ! voir pages 4 et 5

b)  $\dot{Q}_{ea} = ?$  :



i) conservation de la masse :

$$\sum \dot{m}_{in} = \sum \dot{m}_{out}$$

$$\dot{m}_1 + \dot{m}_2 = \dot{m}_3$$

ii) bilan d'énergie (1<sup>ère</sup> loi) :  $\dot{E}_m = \dot{E}_{out}$

$$\dot{m}_1 \theta_1 + \dot{m}_2 \theta_2 = \dot{m}_3 \theta_3 + \dot{Q}_{ea}$$

$$\dot{m}_1 \theta_1 + \dot{m}_2 \theta_2 = (\dot{m}_1 + \dot{m}_2) \theta_3 + \dot{Q}_{ea}$$

$$\dot{Q}_{ea} = \dot{m}_1 (\theta_1 - \theta_3) + \dot{m}_2 (\theta_2 - \theta_3)$$

$$= \dot{m}_1 (h_1 - h_3 + \cancel{\Delta e_{p31}} + \cancel{\Delta e_{c31}})$$

$$+ \dot{m}_2 (h_2 - h_3 + \cancel{\Delta e_{p32}} + \cancel{\Delta e_{c32}})$$

$$\dot{Q}_{ea} = \dot{m}_1 (h_1 - h_3) + \dot{m}_2 (h_2 - h_3)$$

$$= (3.876 \frac{kg}{s}) (3051.6 - 2266.44) \frac{kJ}{kg}$$

$$+ (1 \frac{kg}{s}) (419.17 - 2266.44) \frac{kJ}{kg}$$

$$\dot{Q}_{ea} = 1196.0 \text{ kW}$$

Solution alternative : voir page 4

c)  $v_3 = ?$  :  $\dot{m}_3 = \frac{v_3 A_3}{v_3} = \dot{m}_1 + \dot{m}_2$

$$v_3 = \frac{(\dot{m}_1 + \dot{m}_2) v_3}{A_3}$$

$\Rightarrow v_3 = ?$  :  $P_3 = 1000 \text{ kPa}$  } Table A-5 : pour  $P_{sat} = 1000 \text{ kPa}$   
 $x_3 = 0.7465$  }  $v_f = 0.001127 \frac{m^3}{kg}$   
 $v_g = 0.19436 \frac{m^3}{kg}$

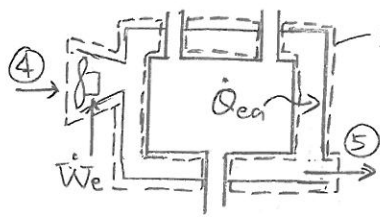
$$v_3 = v_f + x_3 (v_g - v_f)$$

$$= 0.001122 + (0.7465) (0.19436 - 0.001127)$$

$$v_3 = 0.14538 \text{ m}^3/\text{kg}$$

$$v_3 = \frac{(3.876 + 1) \text{ kg/s} (0.14538 \text{ m}^3/\text{kg})}{(0.1 \text{ m}^2)} = 7.089 \frac{m}{s}$$

b)  $\dot{Q}_{ea} = ?$



système = chemise de refroidissement (incluant ventilateur)

i) conservation de la masse

$$\dot{m}_{in} = \dot{m}_{out}$$

$$\dot{m}_4 = \dot{m}_5 = \dot{m}_a$$

ii) bilan d'énergie (1ère loi) :  $\dot{E}_{in} = \dot{E}_{out}$

$$\dot{m}_4 \theta_4 + \dot{W}_e + \dot{Q}_{ea} = \dot{m}_5 \theta_5$$

$$\dot{Q}_{ea} = \dot{m}_a (\theta_5 - \theta_4) - \dot{W}_e$$

$$= \dot{m}_a \left( h_5 - h_4 + \frac{v_5^2 - v_4^2}{2} + \cancel{\Delta e_{p45}} \right) - \dot{W}_e \quad \begin{matrix} \nearrow \approx 0 \\ \nearrow \approx 0 \end{matrix}$$

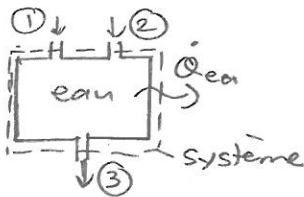
$$= \dot{m}_a \left[ c_p (T_5 - T_4) + \frac{v_5^2 - v_4^2}{2} \right] - \dot{W}_e$$

$$= \left( 30 \frac{\text{kg}}{\text{s}} \right) \left[ \left( 1.005 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right) (60 - 20) \frac{\text{K}}{\text{C}} + \frac{(7^2 - 3^2)}{2} \frac{\text{m}^2}{\text{s}^2} \times \frac{1 \text{kJ}}{10^3 \frac{\text{m}^2}{\text{s}^2}} \right]$$

$$- 10.6 \text{ kW}$$

$$\boxed{\dot{Q}_{ea} = 1196.0 \text{ kW}}$$

a)  $T_3, x_3 = ?$  : On utilise la réponse de (b) pour trouver  $h_3$



i) conservation de la masse

$$\sum \dot{m}_{in} = \sum \dot{m}_{out}$$

$$\dot{m}_1 + \dot{m}_2 = \dot{m}_3$$

ii) bilan d'énergie (1ère loi) :  $\dot{E}_{in} = \dot{E}_{out}$

$$\dot{m}_1 \theta_1 + \dot{m}_2 \theta_2 = \dot{m}_3 \theta_3 + \dot{Q}_{ea}$$

$$\dot{m}_1 \theta_1 + \dot{m}_2 \theta_2 = (\dot{m}_1 + \dot{m}_2) \theta_3 + \dot{Q}_{ea}$$

$$\dot{m}_1 (\theta_3 - \theta_1) + \dot{m}_2 (\theta_3 - \theta_2) = -\dot{Q}_{ea}$$

$$\dot{m}_1 \left( h_3 - h_1 + \cancel{\Delta e_{c13}} + \cancel{\Delta e_{p13}} \right) \quad \begin{matrix} \nearrow \approx 0 \\ \nearrow \approx 0 \end{matrix}$$

$$+ \dot{m}_2 \left( h_3 - h_2 + \cancel{\Delta e_{c23}} + \cancel{\Delta e_{p23}} \right) = -\dot{Q}_{ea} \quad \begin{matrix} \nearrow \approx 0 \\ \nearrow \approx 0 \end{matrix}$$

$$(\dot{m}_1 + \dot{m}_2) h_3 = \dot{m}_1 h_1 + \dot{m}_2 h_2 - \dot{Q}_{ea}$$

$$h_3 = \frac{\dot{m}_1 h_1 + \dot{m}_2 h_2 - \dot{Q}_{ea}}{\dot{m}_1 + \dot{m}_2}$$

$$= \frac{(3.876 \frac{\text{kg}}{\text{s}})(3051.6 \frac{\text{kJ}}{\text{kg}}) + (1 \frac{\text{kg}}{\text{s}})(419.17 \frac{\text{kJ}}{\text{kg}}) - (1196.0 \frac{\text{kJ}}{\text{s}})}{(3.876 + 1) \frac{\text{kg}}{\text{s}}}$$

$$h_3 = 2266.44 \text{ kJ/kg}$$

$$P_3 = 1000 \text{ kPa}$$

$$h_3 = 2266.44 \frac{\text{kJ}}{\text{kg}}$$

} mélange liquide-vapeur saturé

$$T_3 = T_{\text{sat}@1000 \text{ kPa}} = \boxed{179.88^\circ\text{C}}$$

$$x_3 = \frac{h_3 - h_{f@1000 \text{ kPa}}}{(h_g - h_f)@1000 \text{ kPa}} = \boxed{0.7465}$$