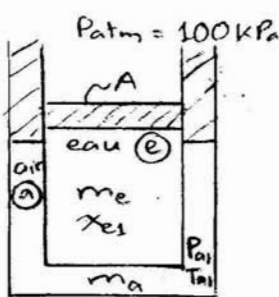
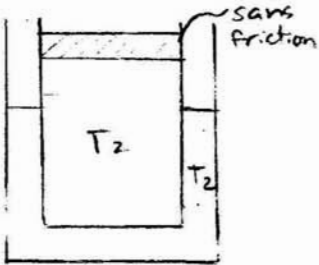


MEC1210 Automne 2024, TD4, Groupe 2: Problème à faire en classe (solutionnaire)



①
 $x_{e1} = 0.5$
 $T_{a1} = 27^\circ\text{C}$
 $P_{a1} = 101 \text{ kPa}$

$P_e \text{ cst}$
 $\bar{V}_a \text{ cst}$
 $A = 0.1 \text{ m}^2$
 $m_e = 0.1 \text{ kg}$
 $m_a = 0.01 \text{ kg}$



②
 équilibre thermique avec rés.
 $T_2 = T_{rés} = 150^\circ\text{C}$

- $M_{\text{piston}} \approx 0$
- air \rightarrow gaz parfait avec $C_p, C_v \text{ const}$
- $R = 0.287 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$
- $C_p = 1.005 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$
- $\Delta U_{\text{paroi, piston, gaz}} \approx 0$ (chauds)
- $\Delta S_{\text{paroi, piston, gaz}} \approx 0$ (chauds)
- Isolants parfaits ($Q_{\text{out}} = 0$)
- $\Delta E_c, \Delta E_p \approx 0$
- évolution quasi-statique

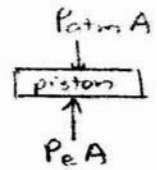
- a) $\Delta z = ?$
 b) $Q = ?$
 c) $S_{\text{gen}} = ?$
 d) diagramme T-s pour air et eau

Suppositions additionnelles
 (aucune)

a) $\Delta z = ? : A\Delta z = \bar{V}_{e2} - \bar{V}_{e1} = m_e (v_{e2} - v_{e1})$

$$\Delta z = \frac{m_e}{A} (v_{e2} - v_{e1})$$

$\Rightarrow v_{e1} = ? : P_{e1} = ? :$



$\sum F_z = P_e A - P_{atm} A = 0$ (quasi-statique)
 $P_e = P_{atm} = \text{const.}$

$P_{e1} = P_{e2} = P_{atm} = 100 \text{ kPa}$

$P_{e1} = 100 \text{ kPa}$ } mélange sat.
 $x_{e1} = 0.5$ } Table A-5: $v_f = 0.001043 \frac{\text{m}^3}{\text{kg}}$
 $P_{\text{sat}} = 100 \text{ kPa}$ } $v_g = 1.6941 \frac{\text{m}^3}{\text{kg}}$
 $u_f = 417.40 \frac{\text{kJ}}{\text{kg}}$ } $s_f = 1.3028 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$
 $u_{fg} = 2088.2 \frac{\text{kJ}}{\text{kg}}$ } $s_{fg} = 6.0562 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$

$v_{e1} = v_f + x_{e1}(v_g - v_f) = 0.8475 \text{ m}^3/\text{kg}$
 $u_{e1} = u_f + x_{e1}u_{fg} = 1461.5 \frac{\text{kJ}}{\text{kg}}$
 $s_{e1} = s_f + x_{e1}s_{fg} = 4.3309 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$

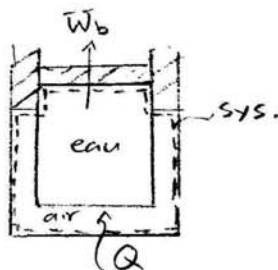
$$\Rightarrow v_{e2} = ? : \left. \begin{array}{l} P_{e2} = P_{e1} = 100 \text{ kPa} \\ T_{e2} = T_2 = 150^\circ\text{C} \end{array} \right\} \begin{array}{l} T_{e2} > T_{\text{sat}@100\text{kPa}} \\ \text{vap. sur.} \end{array}$$

Table A-6: $v_{e2} = 1.9367 \text{ m}^3/\text{kg}$
 $(u_{e2} = 2582.9 \text{ kJ/kg})$
 $(s_{e2} = 7.6148 \text{ kJ/kg}\cdot\text{K})$

$$\Delta z = \frac{(0.1 \text{ kg}) (1.9367 - 0.8476) \frac{\text{m}^3}{\text{kg}}}{(0.1 \text{ m}^2)}$$

$$\Delta z = 1.0891 \text{ m}$$

b) $Q = ? :$



bilan d'énergie: $\Delta E_{\text{sys}} = E_m - E_{\text{out}}$
(1ère loi)

$$\Delta U_{\text{eau}} + \Delta U_{\text{air}} + \Delta U_{\text{piston}} + \Delta E_c + \Delta E_p = Q - W_b$$

$\begin{matrix} \nearrow = 0 & \nearrow = 0 & \nearrow = 0 \\ \searrow & \searrow & \searrow \end{matrix}$

$$m_e (u_{e2} - u_{e1}) + m_a (u_{a2} - u_{a1}) = Q - \int_{\text{①}}^{\text{②}} P_e dV$$

$$m_e (u_{e2} - u_{e1}) + m_a c_{va} (T_2 - T_{a1}) = Q - P_{e1} m_e (v_{e2} - v_{e1})$$

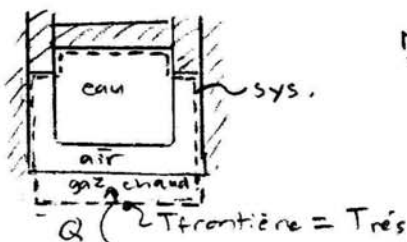
$$Q = m_e [u_{e2} - u_{e1} + P_e (v_{e2} - v_{e1})] + m_a c_{va} (T_2 - T_{a1})$$

$$\Rightarrow c_{va} = c_{pa} - R = 1.005 - 0.287 = 0.722 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$$

$$= (0.1 \text{ kg}) \left[(2582.9 - 1461.5) \frac{\text{kJ}}{\text{kg}} + (100 \text{ kPa}) (1.9367 - 0.8476) \frac{\text{m}^3}{\text{kg}} \right] + (0.01 \text{ kg}) (0.722 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}) (150 - 27)^\circ\text{C} \cdot \frac{\text{K}}{^\circ\text{C}}$$

$$Q = 123.92 \text{ kJ}$$

c) $S_{\text{gen}} = ? :$



Note: système doit s'étendre en bas jusqu'à ce que $T_{\text{frontière}} = T_{\text{rés}} = \text{const.}$ pour que S_{gen} inclut irréversibilité due à Q à travers $\Delta T = T_{\text{rés}} - T_{\text{air}}$

bilan d'entropie : $\Delta S_{sys} = \int \frac{\delta Q}{T} + S_{gen}$
 (2ème loi)

$\Delta S_{eau} + \Delta S_{air} + \Delta S_{\substack{\text{parois} \\ \text{\& air} \\ \text{chauds}}} = \frac{Q}{T_{rés}} + S_{gen}$

$m_e (s_{e2} - s_{e1}) + m_a (s_{a2} - s_{a1}) = \frac{Q}{T_{rés}} + S_{gen}$

$S_{gen} = m_e (s_{e2} - s_{e1}) + m_a (s_{a2} - s_{a1}) - \frac{Q}{T_{rés}}$

$\Rightarrow s_{a2} - s_{a1} = C_{va} \ln \frac{T_2}{T_{a1}} + R \ln \frac{v_{a2}}{v_{a1}}$ (gaz parfait avec c_v, c_p const.)
 $= (0.722 \frac{kJ}{kg \cdot K}) \ln \left(\frac{150 + 273}{27 + 273} \right) + 0$
 $= 0.2481 \text{ kJ/kg} \cdot K$

ou
 $s_{a2} - s_{a1} = C_{pa} \ln \frac{T_2}{T_{a1}} - R \ln \frac{P_{a2}}{P_{a1}}$

$\Rightarrow \frac{P_{a2}}{P_{a1}} = \frac{RT_2/v_{a2}}{RT_{a1}/v_{a1}} = \frac{T_2}{T_{a1}}$

$s_{a2} - s_{a1} = \underbrace{(C_{pa} - R)}_{C_{va}} \ln \frac{T_2}{T_{a1}} = \text{même qu'avant}$

$S_{gen} = (0.1 \text{ kg}) (7.6148 - 4.3309) \frac{kJ}{kg} + (0.01 \text{ kg}) (0.2481 \frac{kJ}{kg \cdot K})$
 $= \frac{-123.92 \text{ kJ}}{(150 + 273) \text{ K}}$

$S_{gen} = 0.038 \frac{kJ}{K}$

